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APPENDICES

Appendix A Temperature-programmed Desorption (TPD)

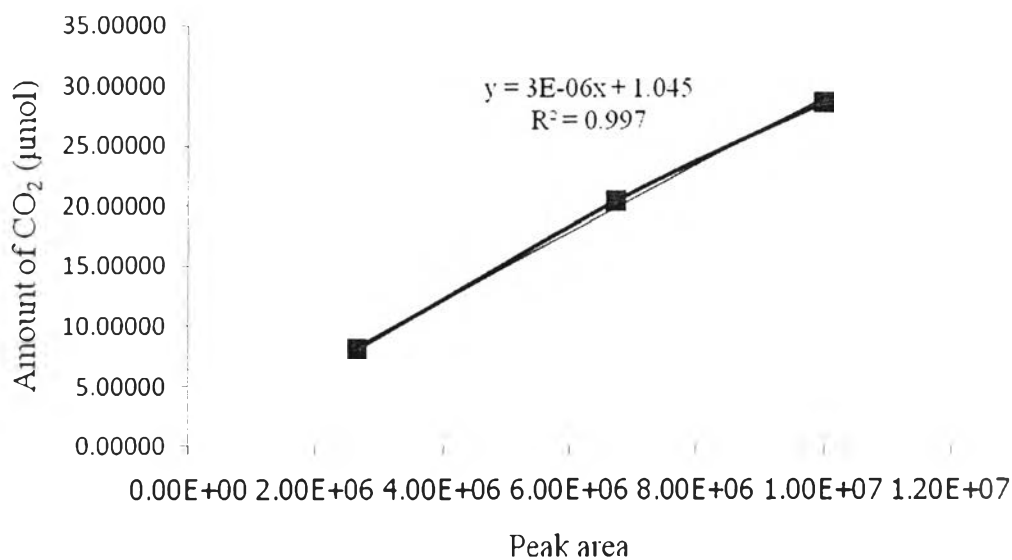


Figure A1 Calibration curve of CO₂ Temperature-programmed desorption (CO₂-TPD).

Table A1 The results for calculation the amount of CO₂ from TPD

P (atm)	V (ml)	R (Latm/Kmol)	T (K)	Amount of CO ₂ (µmol)	Peak Area	Average Peak
1	0.2	0.082507	298	8.17896	2.68E+06	2.64E+06
1	0.2	0.082507	298	8.17896	2.63E+06	
1	0.2	0.082507	298	8.17896	2.61E+06	
1	0.5	0.082507	298	20.44740	6.94E+06	6.71E+06
1	0.5	0.082507	298	20.44740	6.68E+06	
1	0.5	0.082507	298	20.44740	6.51E+06	
1	0.7	0.082507	298	28.62636	1.01E+07	9.96E+06
1	0.7	0.082507	298	28.62636	9.99E+06	
1	0.7	0.082507	298	28.62636	9.86E+06	

P = Pressure, V= Volume of gas, R = Gas constant, T = Absolute temperature

Table A2 Calculation the basic site of catalysts

Sample	Weight of Sample	Area of Sample	Temperature Desorption (°C)	Amount of CO ₂ (μmol/g)
NaY	0.1047	4.20E+07	184	1203.15
5 %K/NaY	0.1142	3.45E+07	154	905.25
10 %K/NaY	0.1104	1.37E+07	210	372.55
	0.1104	2.39E+06	398	64.94
15 %K/NaY	0.1120	1.90E+06	222	50.89
	0.1120	1.33E+07	397	356.25
20 %K/NaY	0.1000	1.24E+07	399	372.00

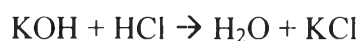
Appendix B Acid Titration Method

1. Standardization of KOH was measured by using potassium acid phthalate (titration grade)

$$\text{Normality} = (W_p * 1000) / (MW * (V - V_b))$$

Where W_p = Weight of potassium acid phthalate (g)
 V = Amount of KOH was used in titration sample (ml)
 V_b = Amount of KOH was used in titration blank (ml)
 MW = Molecular weight of potassium acid phthalate

2. A 0.02 M of KOH solution was used to measure the concentration of HCl solution.



3. To evaluate the basicity of catalysts, the remained HCl in the solution was calculated.

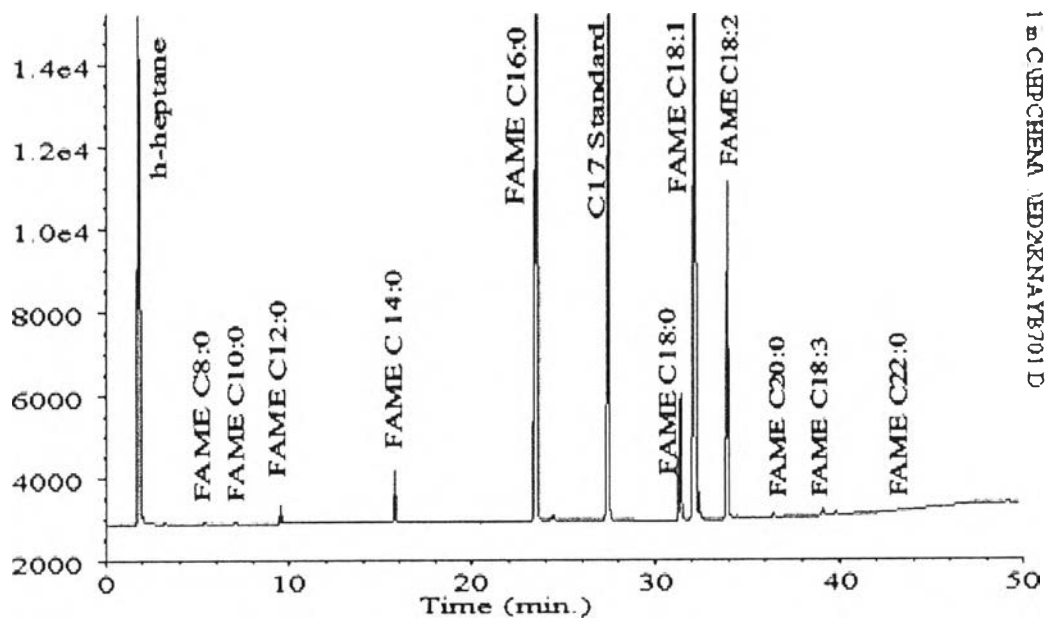
Table B1 Calculation the basic site of catalysts

Sample	No.	Volume (ml)		KOH (ml)	HCl (ml)	Weight of Catalyst	Back Titration	Total Basic Site (mmol)	Total Basic Site (mmol/g)	Avg.
		Start	Final							
Bentonite	1	10	13.95	3.95	5	0.1005	2.25	0.0476	0.473	0.475
	2	10	13.9	3.9	5	0.102	2.3	0.0486	0.476	
5 %K/bentonite	1	13	13.55	0.55	5	0.1008	5.65	0.1195	1.185	1.192
	2	14	14.45	0.45	5	0.1015	5.75	0.1216	1.198	

Appendix C Gas Chromatography (GC)

Table C1 Calculation of the methyl ester yield and weight of palm oil

Free Fatty Acid	Molecular	Molecular weight (X1)	Methyl ester (wt%) (X2)	(X1 x X2)
caprylic (C8:0)	C ₂₇ H ₅₀ O ₂	470	0.01	0.05
carpic (C10:0)	C ₃₃ H ₆₂ O ₂	554	0.01	0.06
Lauric (C12:0)	C ₃₉ H ₇₄ O ₂	638	0.20	1.28
Myristic (C14:0)	C ₄₅ H ₈₆ O ₂	722	0.83	5.99
Palmitic (C16:0)	C ₅₁ H ₉₈ O ₂	806	40.29	324.74
Stearic (C18:0)	C ₅₇ H ₉₆ O ₂	890	3.70	32.93
Oleic (C18:1)	C ₅₇ H ₉₄ O ₂	884	43.73	386.57
Linoleic (C18:2)	C ₅₇ H ₉₂ O ₂	878	10.64	93.42
Linolenic (C18:3)	C ₅₇ H ₉₀ O ₂	872	0.19	1.66
Arachidic (C20:0)	C ₆₃ H ₁₂₂ O ₂	974	0.30	2.92
Total			100	849.61



Sg 1 m CHERCHEM \ED2AKNAYR701 D

Figure C1 Chromatogram of fatty acid methyl ester (FAMES) in biodiesel.

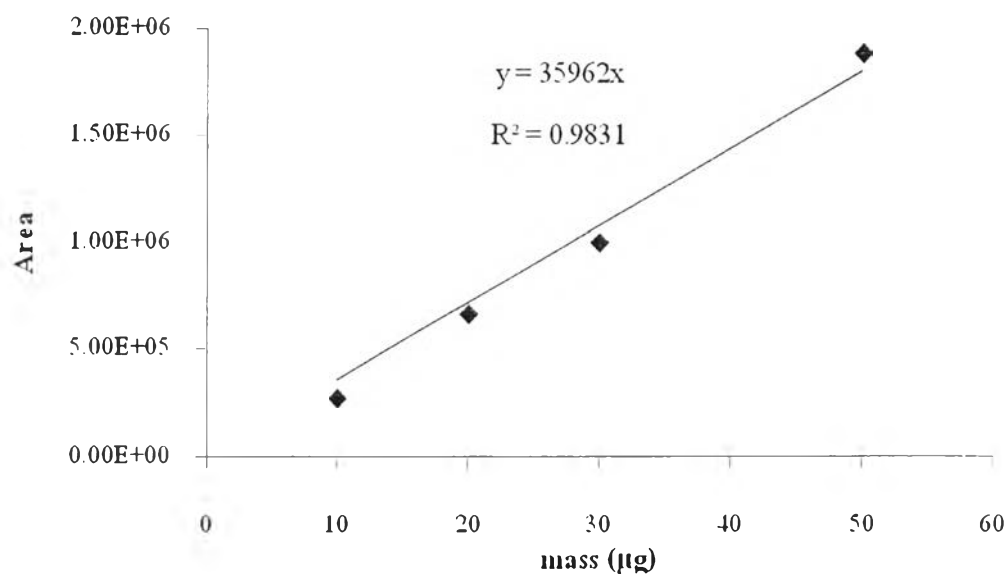


Figure D1 Standard curve of 1-monooleoly-rac-glycerol (C18:1-cis-9), Purity > 99%.

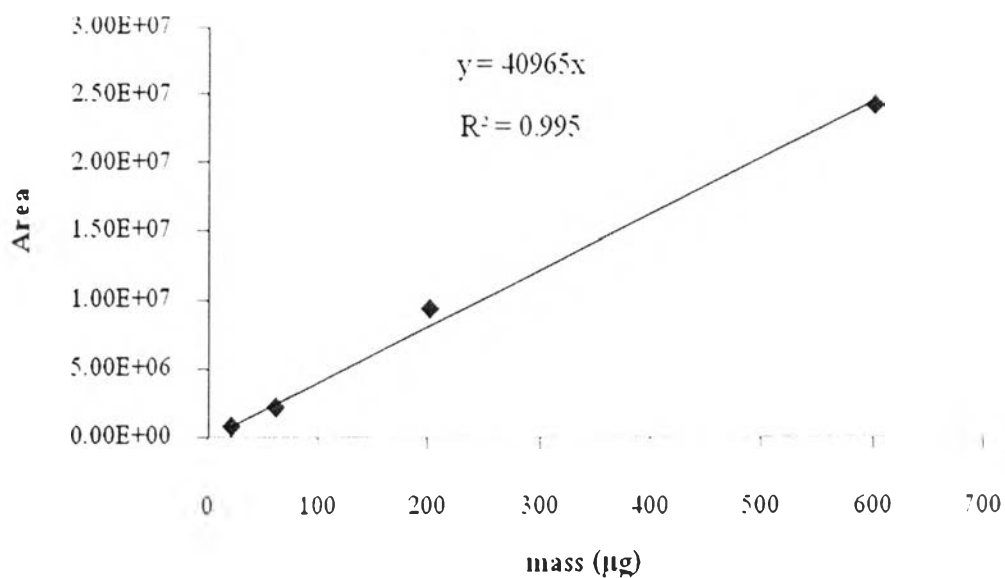


Figure D2 Standard curve of methyl ester of oleic acid (C18:1), Purity > 99%.

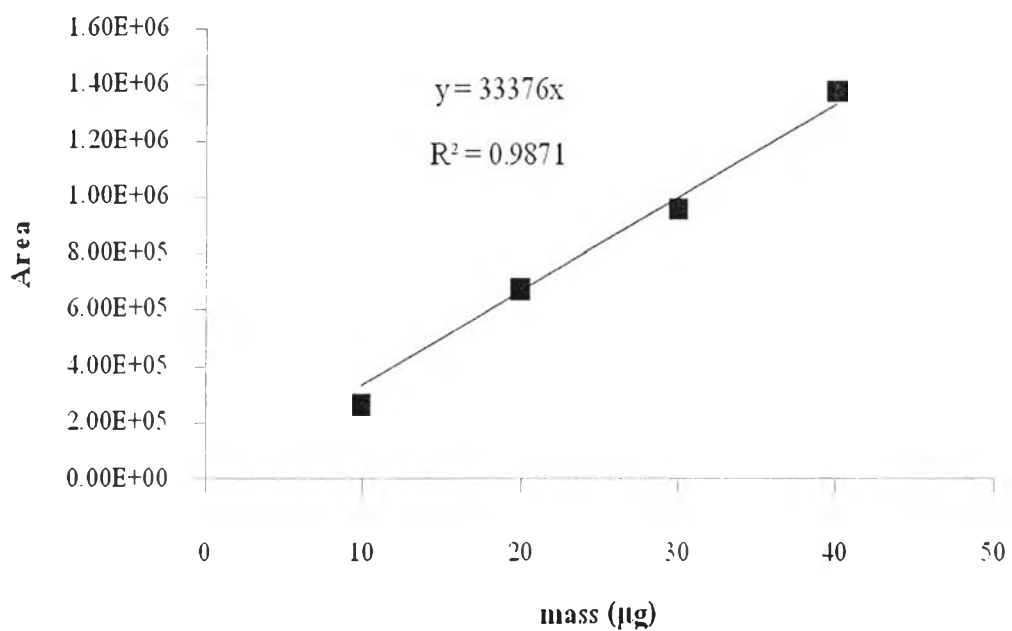


Figure D3 Standard curve of 1, 3-diolein (C18:1-cis-9), Purity > 99%.

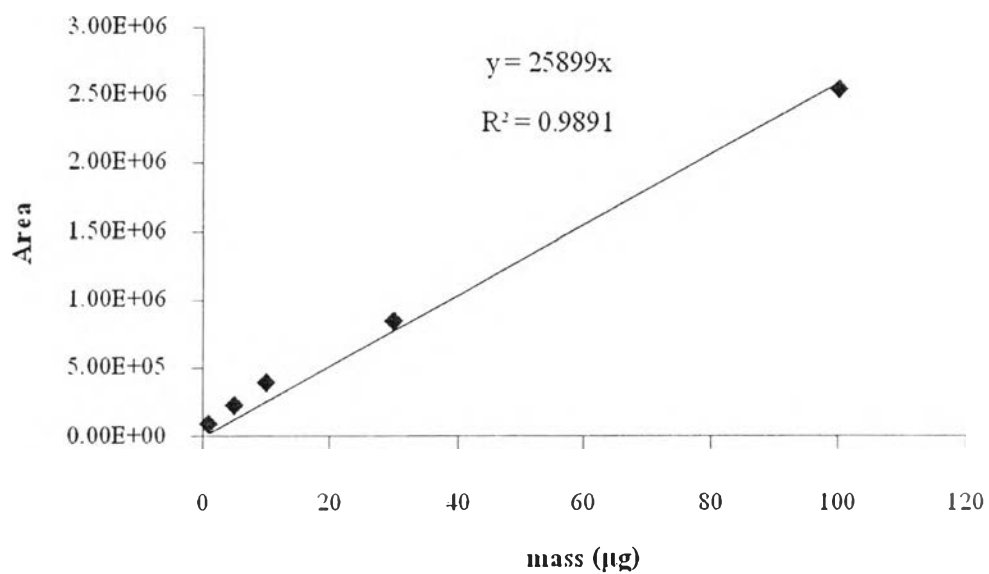


Figure D4 Standard curve of triolein (C18:1), Purity > 99%.

Table D1 Correlation coefficient of calibration curves in HPLC from standard solution

Sample	Retention time (minutes)	Slope (mV/ μ g)	Correlation coefficient	R _f *
1-monooleoly (C18:1-cis-9)	2-4	33965	0.983	32878.44
Methyl ester of oleic acid (C18:1)	5-10	40965	0.995	41420.50
1, 3-diolein (C18:1-cis-9)	10-15	33376	0.987	31699.30
triolein (C18:1)	16-25	25899	0.989	47849.84

*Response factor = (area of standard)/ (amount of standard)

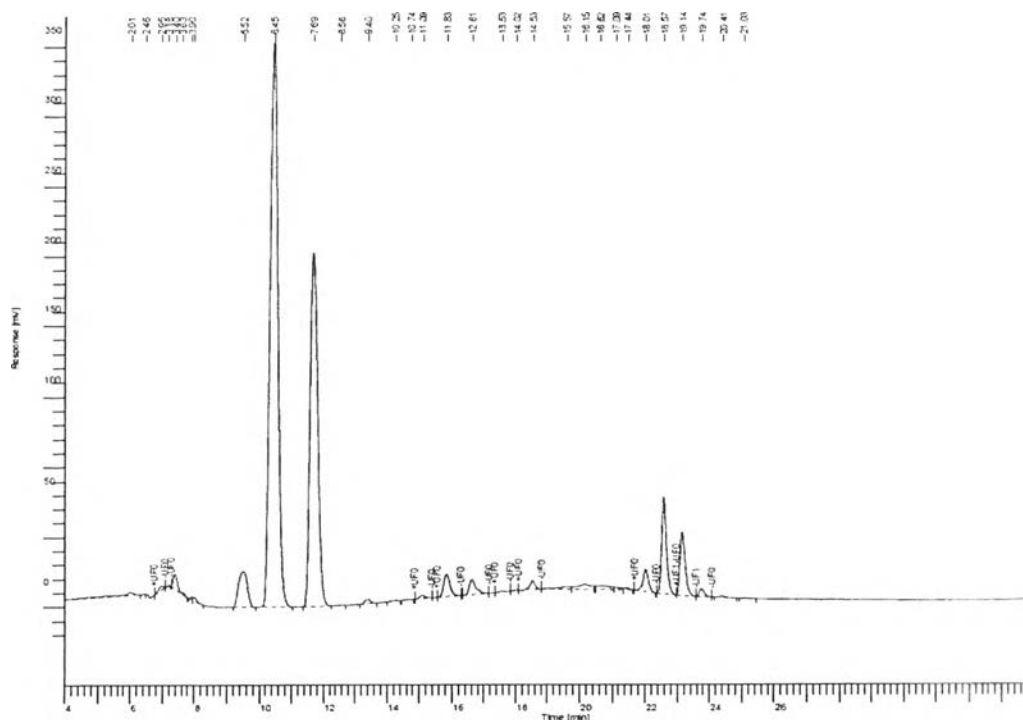


Figure D5 HPLC chromatogram of mono-, di-, tri-glycerol, and biodiesel (methyl ester 74.5 % from GC).

Table D2 Calculation of mono-, di-, tri-glyceride and methyl ester yield of biodiesel

Time	Area	Height	Area	Composition		*Sum	wt (%)
2.457	810.41	167.4	0.01	C14:0	0.022535	Mono- 4.932	1.55
2.947	31834.33	3049.31	0.23	C18:3	0.885221		
3.18	4847.54	977.64	0.03	C18:2	0.134796		
3.395	99580.8	10314.97	0.71	C18:1	2.769056		
3.626	11475.2	1192.52	0.08	C16:0	0.319092		
3.902	9316.88	1875.06	0.07	C18:0	0.259076		
3.975	20334.72	2496.97	0.14	C20:0	0.56545		
5.521	484104	25700.9	3.43	-	11.8175	FAME 233.841	73.53
6.451	5812095	403935.6	48.33	-	141.8795		
7.689	3244816	251965.4	30.11	-	79.20947		
9.398	38298	3125.81	0.27	-	0.934896		
10.247	7423.8	610.79	0.05	C14:0	0.222429	di- 12.760	4.01
10.742	2951.2	161.3	0.02	C18:3	0.088423		
11.087	28433.56	2297.14	0.2	C18:2	0.851916		
11.833	214535.5	15761.23	1.52	C18:1	6.427839		
12.613	161418.1	11047.4	1.15	C16:0	4.836353		
13.533	8142.72	936.31	0.06	C18:0	0.243969		
14.017	2983.4	382.89	0.02	C20:0	0.089388		
14.527	70286.07	6242.07	0.5	C10:0	2.713853	Tri- 63.697	20.03
15.575	53674.8	1788.61	0.38	C12:0	2.072466		
17.086	24592.58	1684.21	0.17	C14:0	0.949557		
17.444	13198.57	1296.13	0.09	C18:3	0.509617		
18.007	178985.9	15866.27	1.27	C18:2	6.91092		
18.573	717077.2	69490.66	5.09	C18:1	27.68745		
19.142	514495.8	45623.4	3.65	C16:0	19.86547		
19.74	62423.01	5838.59	0.44	C18:0	2.410248		
20.408	12478	958.99	0.09	C20:0	0.481795		
21.029	2497.2	185.39	0.02	C24:0	0.096421		

* Mono-, di-, tri-glyceride and methyl ester

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1. Noiroj, K., Intarapong, P., Luengnaruemitchai, A. and Jai-In, S. (2009) A comparative study of KOH/Al₂O₃ and KOH/NaY catalysts for biodiesel production via transesterification from palm oil. Renewable Energy, 34(4), 1145–1150.
2. Intarapong, P., Luengnaruemitchai, A. and Jai-In, S. (2011) Transesterification of palm oil over KOH/NaY zeolite in a packed-bed reactor. Journal of Renewable Energy Research, 4, 271–280.
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4. Intarapong, P., Iangthanarat, S., Phanthong, P., Luengnaruemitchai, A. and Jai-In, S. (2013) Activity and basic properties of KOH/mordenite for transesterification of palm oil. Journal of Energy Chemistry, in revision.
5. Intarapong, P., Luengnaruemitchai, A. and Jai-In, S. (2013) Transesterification of palm oil using KOH supported on bentonite in a continuous reactor. International Journal of Green Energy, in revision.

Proceedings:

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3. Intarapong, P.; Luengnaruemitchai, A.; and Jai-In, S. (2011, March 26-31) Transesterification of palm oil using KOH loading on various type of support in a continuous flow reactor. Paper presented at the 24^{1st} ACS National Meeting 2011, Anaheim, CA, USA.